



$${}^{\alpha}\Delta^{\beta}\mu = \mu_j(\alpha) - \mu_j(\beta) = 0$$

$$\mu_j(\alpha) = \mu_j(\beta)$$

Physical and Interfacial Electrochemistry 2013

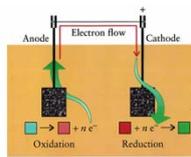


Figure 18.7
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Lecture 4. Electrochemical Thermodynamics

Module JS CH3304 Molecular Thermodynamics and Kinetics

Thermodynamics of electrochemical systems

Thermodynamics, the science of possibilities is of general utility. The well established methods of thermodynamics may be readily applied to electrochemical cells.

We can readily compute thermodynamic state functions such as ΔG , ΔH and ΔS for a chemical reaction by determining how the open circuit cell potential E_{cell} varies with solution temperature.

We can compute the thermodynamic efficiency of a fuel cell provided that ΔG and ΔH for the cell reaction can be evaluated.

We can also use measurements of equilibrium cell potentials to determine the concentration of a redox active substance present at the electrode/solution interface. This is the basis for potentiometric chemical sensing.

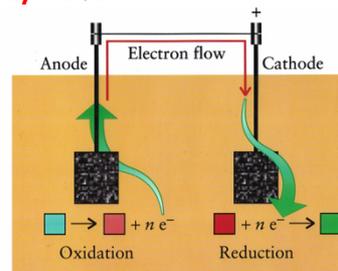
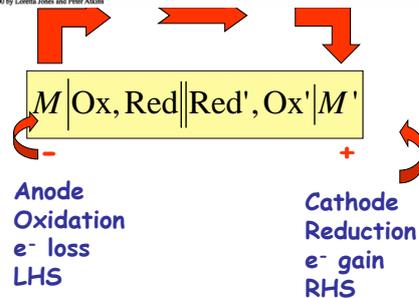


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Standard Electrode Potentials

Standard reduction potential (E^0) is the voltage associated with a **reduction reaction** at an electrode when all solutes are 1 M and all gases are at 1 atm.



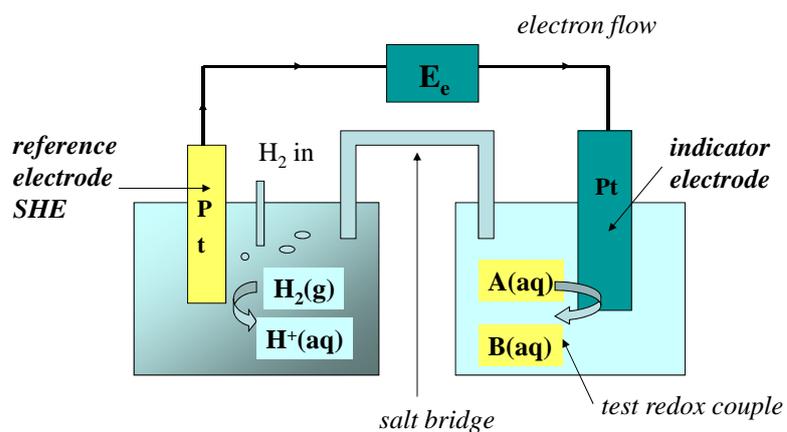
Reduction Reaction



$$E^0 = 0\text{ V}$$

Standard hydrogen electrode (SHE)

Measurement of standard redox potential E^0 for the redox couple $A(aq)/B(aq)$.



E^0 provides a quantitative measure for the thermodynamic tendency of a redox couple to undergo reduction or oxidation.

Table 19.1 Standard Reduction Potentials at 25°C*

Half-Reaction	E^\ominus (V)
$F_2(g) + 2e^- \rightarrow 2F^-(aq)$	+2.87
$O_2(g) + 2H^+(aq) + 2e^- \rightarrow O_2(g) + H_2O$	+2.07
$Co^{3+}(aq) + e^- \rightarrow Co^{2+}(aq)$	+1.82
$H_2O_2(aq) + 2H^+(aq) + 2e^- \rightarrow 2H_2O$	+1.77
$PbO_2(s) + 4H^+(aq) + SO_4^{2-}(aq) + 2e^- \rightarrow PbSO_4(s) + 2H_2O$	+1.70
$Ce^{4+}(aq) + e^- \rightarrow Ce^{3+}(aq)$	+1.61
$MnO_4^-(aq) + 8H^+(aq) + 5e^- \rightarrow Mn^{2+}(aq) + 4H_2O$	+1.51
$Au^{3+}(aq) + 3e^- \rightarrow Au(s)$	+1.50
$Cl_2(g) + 2e^- \rightarrow 2Cl^-(aq)$	+1.36
$Cr_2O_7^{2-}(aq) + 14H^+(aq) + 6e^- \rightarrow 2Cr^{3+}(aq) + 7H_2O$	+1.33
$MnO_2(s) + 4H^+(aq) + 2e^- \rightarrow Mn^{2+}(aq) + 2H_2O$	+1.23
$O_2(g) + 4H^+(aq) + 4e^- \rightarrow 2H_2O$	+1.23
$Br_2(l) + 2e^- \rightarrow 2Br^-(aq)$	+1.07
$NO_3^-(aq) + 4H^+(aq) + 3e^- \rightarrow NO(g) + 2H_2O$	+0.96
$2Hg^{2+}(aq) + 2e^- \rightarrow 2Hg(l)$	+0.92
$Hg_2^{2+}(aq) + 2e^- \rightarrow 2Hg(l)$	+0.85
$Ag^+(aq) + e^- \rightarrow Ag(s)$	+0.80
$Fe^{3+}(aq) + e^- \rightarrow Fe^{2+}(aq)$	+0.77
$O_2(g) + 2H^+(aq) + 2e^- \rightarrow H_2O_2(aq)$	+0.68
$MnO_4^-(aq) + 2H_2O + 3e^- \rightarrow MnO_2(s) + 4OH^-(aq)$	+0.59
$I_2(s) + 2e^- \rightarrow 2I^-(aq)$	+0.53
$O_2(g) + 2H_2O + 4e^- \rightarrow 4OH^-(aq)$	+0.40
$Cu^{2+}(aq) + 2e^- \rightarrow Cu(s)$	+0.34
$AgCl(s) + e^- \rightarrow Ag(s) + Cl^-(aq)$	+0.22
$SO_4^{2-}(aq) + 4H^+(aq) + 2e^- \rightarrow SO_2(g) + 2H_2O$	+0.20
$Cu^{2+}(aq) + e^- \rightarrow Cu^+(aq)$	+0.15
$Sn^{4+}(aq) + 2e^- \rightarrow Sn^{2+}(aq)$	+0.13
$2H^+(aq) + 2e^- \rightarrow H_2(g)$	0.00
$Pb^{2+}(aq) + 2e^- \rightarrow Pb(s)$	-0.13
$Sr^{2+}(aq) + 2e^- \rightarrow Sr(s)$	-0.14
$Ni^{2+}(aq) + 2e^- \rightarrow Ni(s)$	-0.25
$Co^{2+}(aq) + 2e^- \rightarrow Co(s)$	-0.28
$PbSO_4(s) + 2e^- \rightarrow Pb(s) + SO_4^{2-}(aq)$	-0.31
$Cd^{2+}(aq) + 2e^- \rightarrow Cd(s)$	-0.40
$Fe^{2+}(aq) + 2e^- \rightarrow Fe(s)$	-0.44
$Cr^{3+}(aq) + 3e^- \rightarrow Cr(s)$	-0.74
$Zn^{2+}(aq) + 2e^- \rightarrow Zn(s)$	-0.76
$2H_2O + 2e^- \rightarrow H_2(g) + 2OH^-(aq)$	-0.83
$Mn^{2+}(aq) + 2e^- \rightarrow Mn(s)$	-1.18
$Al^{3+}(aq) + 3e^- \rightarrow Al(s)$	-1.66
$Ba^{2+}(aq) + 2e^- \rightarrow Ba(s)$	-1.85
$Mg^{2+}(aq) + 2e^- \rightarrow Mg(s)$	-2.37
$Na^+(aq) + e^- \rightarrow Na(s)$	-2.71
$Ca^{2+}(aq) + 2e^- \rightarrow Ca(s)$	-2.87
$Sr^{2+}(aq) + 2e^- \rightarrow Sr(s)$	-2.89
$Ba^{2+}(aq) + 2e^- \rightarrow Ba(s)$	-2.90
$K^+(aq) + e^- \rightarrow K(s)$	-2.93
$Li^+(aq) + e^- \rightarrow Li(s)$	-3.05

*For all half-reactions the concentration is 1 M for dissolved species and the pressure is 1 atm for gases. These are the standard state values.

Standard electrode potential

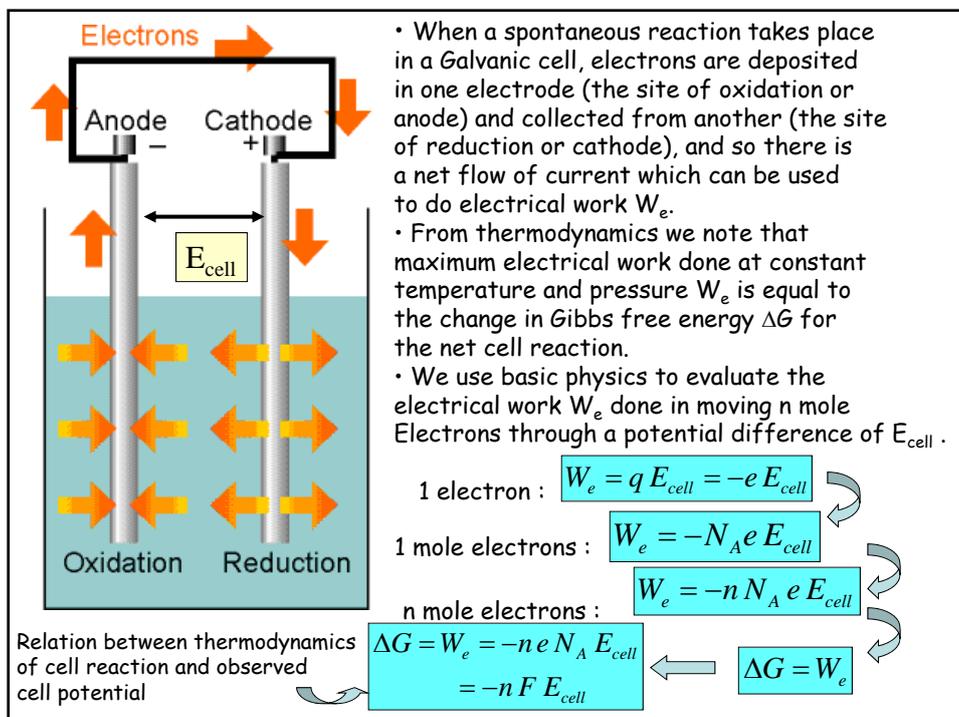
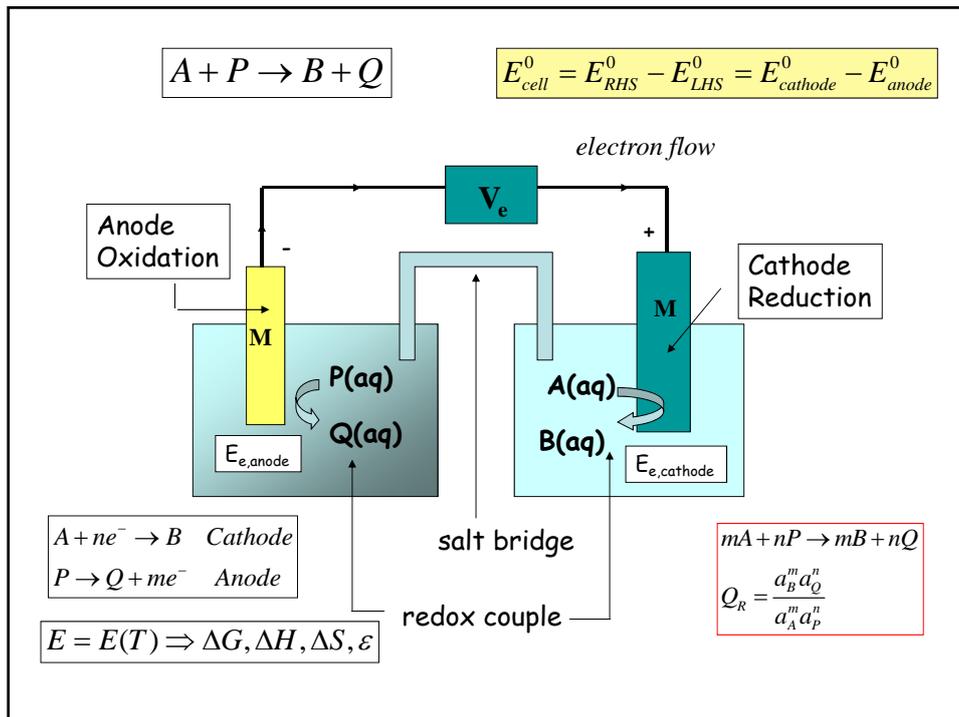
- E^\ominus is for the reaction as written
- The more positive E^\ominus the greater the tendency for the substance to be reduced
- The half-cell reactions are reversible
- The sign of E^\ominus changes when the reaction is reversed
- Changing the stoichiometric coefficients of a half-cell reaction **does not** change the value of E^\ominus

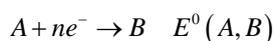
19.3

We should recall from our CH1101 electrochemistry lectures that any combination of two redox couples may be used to fabricate a galvanic cell. This facility can then be used to obtain useful thermodynamic information about a cell reaction which would be otherwise difficult to obtain. Herein lies the usefulness of electrochemical thermodynamics.

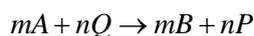
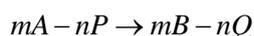
Given any two redox couples A/B and P/Q we can readily use tables of standard reduction potentials to determine which of the two couples is preferentially reduced. Once this is known the galvanic cell can be constructed, the net cell potential can be evaluated, and knowing this useful thermodynamic information can be obtained for the cell reaction.

The procedure is simple to apply. One determines the couple with the most positive standard reduction potential (or the most positive equilibrium potential E_e determined via the Nernst equation if the concentrations of the reactants differ from 1 mol dm⁻³). This couple will undergo reduction at the cathode. The other redox couple will consequently undergo oxidation at the anode. This information can also be used to determine the direction of electron flow, for upon placing a load on the cell electrons will flow out of the anode because of the occurrence of a spontaneous de-electronation (otherwise known as oxidation or electron loss) reaction, through the external circuit and into the cathode causing a spontaneous electronation (aka reduction or electron gain) reaction to occur. Hence in a driven cell the **anode** will be the **negative** pole of the cell and the **cathode** the **positive** pole. Now according to the IUPAC convention if the cell reaction is spontaneous the resultant cell potential will be positive. We ensure that such is the case by writing the cathode reaction on the rhs, and the anode reaction on the lhs of the cell diagram. Then since $E_{e, rhs}$ is more positive than $E_{e, lhs}$ a positive cell potential V_e will be guaranteed.





We subtract the two reactions to obtain the following result.

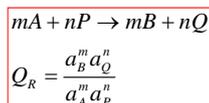
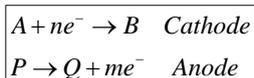


To proceed we subtract the corresponding thermodynamic state functions
In this case ΔG^0

$$\Delta G_{cell}^0 = m\Delta G_{A,B}^0 - n\Delta G_{P,Q}^0 = m(-nFE_{A,B}^0) - (-mFE_{P,Q}^0) = -nmF\{E_{A,B}^0 - E_{P,Q}^0\} = -nmFE_{cell}^0$$

Note that nm denotes the number of electrons transferred per mole of reaction as written.

Net Cell Reaction



The establishment of equilibrium does not imply the cessation of redox activity at the interface .

The condition of equilibrium implies an equality in the electrochemical potentials of the transferring species in the two phases and in the establishment of a compensating two way flow of charge across the interface resulting in a definite **equilibrium potential difference** $\Delta\phi_e$ or E_e .

A single equilibrium potential difference may not be measured.

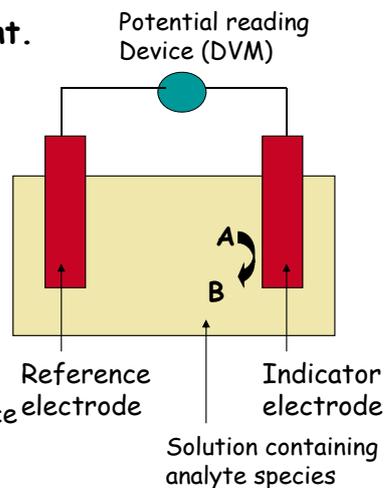
Instead a potential is measured between two electrodes (a test or indicator electrode and a reference electrode).

This is a *potentiometric* measurement.

The potential of the indicator electrode is related to the activities of one or more of the components of the test solution and it therefore determines the overall equilibrium cell potential E_e . Under ideal circumstances, the response of the indicator electrode to changes in analyte species activity at the indicator electrode/solution interface should be rapid, reversible and governed by the Nernst equation. The ET reaction involving the analyte species should be kinetically facile and the ratio of the analyte/product concentration should depend on the interfacial potential difference via the Nernst equation.

The potentiometric measurement.

In a potentiometric measurement two electrodes are used. These consist of the **indicator** or sensing electrode, and a **reference** electrode. Electroanalytical measurements relating potential to analyte concentration rely on the response of one electrode only (the indicator electrode). The other electrode, the reference electrode is independent of the solution composition and provides A stable constant potential. The open circuit cell potential is measured using a potential measuring device such as a potentiometer, a high impedance voltmeter or an electrometer.



Equilibrium condition between phases: chemical potential.

It is well known from basic chemical thermodynamics that if two phases α and β with a common uncharged species j , are brought together, then the tendency of species j to pass from phase α to phase β will be determined by the difference ${}^{\alpha}\Delta^{\beta}\mu$ in the chemical Potential between the two phases.

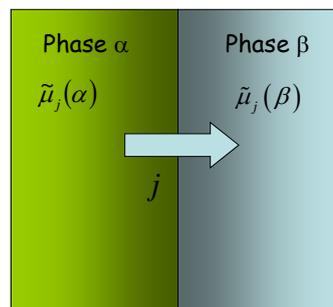
The condition for equilibrium is

$$\begin{aligned} {}^{\alpha}\Delta^{\beta}\mu &= \mu_j(\alpha) - \mu_j(\beta) = 0 \\ \mu_j(\alpha) &= \mu_j(\beta) \end{aligned}$$

The standard thermodynamic definition of the chemical potential is:

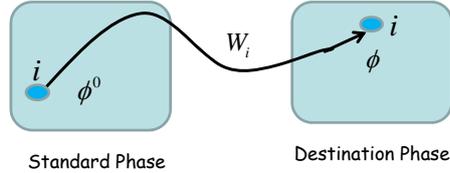
$$\mu_j(\alpha) = \left(\frac{\partial G}{\partial n_j} \right)_{n_i, P, T}$$

Alternatively we can view the chemical potential of a species j in a phase α as a measure of the work that must be done for the reversible transfer of one mole of uncharged species j from the gaseous state of unit fugacity (the reference state) into the bulk of phase α . In electrochemistry we deal with charged species and charged phases.



Electrochemical Activity

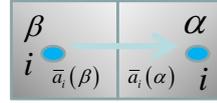
We consider the work done W_i in transferring a species i from the interior of a standard phase to the interior of the phase of interest. We also assume that the species i has a charge $q_i = z_i e$.



The electrochemical activity can be defined in the following manner.

$$\bar{a}_i = a_i \exp \left[\frac{q_i}{k_B T} (\phi - \phi^0) \right] = a_i \exp \left[\frac{z_i F}{RT} (\phi - \phi^0) \right] = \exp \left[\frac{W_i}{k_B T} \right]$$

In the latter expression a_i represents the activity of species i .



If two phases α and β contain a species i with different electrochemical activities such that the electrochemical activity of species i in phase β is greater than that of phase α then there is a tendency for species i to leave phase β and enter phase α . The driving force for the transport of species i is the difference in electrochemical activity between the two phases.

Now from the definition of electrochemical activity

$$\bar{a}_i(\beta) = a_i(\beta) \exp \left[\frac{z_i F}{RT} (\phi_\beta - \phi^0) \right]$$

$$\bar{a}_i(\alpha) = a_i(\alpha) \exp \left[\frac{z_i F}{RT} (\phi_\alpha - \phi^0) \right]$$

Hence

$$\frac{\bar{a}_i(\beta)}{\bar{a}_i(\alpha)} = \frac{a_i(\beta)}{a_i(\alpha)} \exp \left[\frac{z_i F}{RT} (\phi_\beta - \phi_\alpha) \right]$$

$$= \frac{a_i(\beta)}{a_i(\alpha)} \exp \left[\frac{z_i F}{RT} \Delta_{\alpha\beta} \phi \right]$$

We can follow the lead of Lewis and introduce the difference in electrochemical potential as follows.

$$\Delta \bar{\mu}_i = \bar{\mu}_i(\beta) - \bar{\mu}_i(\alpha)$$

We can immediately deduce a relationship between the electrochemical potential difference and the ratio of electrochemical activities between two phases α and β via the following relationships.

$$\Delta \bar{\mu}_i = RT \ln \left\{ \frac{\bar{a}_i(\beta)}{\bar{a}_i(\alpha)} \right\} = RT \ln \left\{ \frac{a_i(\beta)}{a_i(\alpha)} \right\} + z_i F \Delta_{\alpha\beta} \phi$$

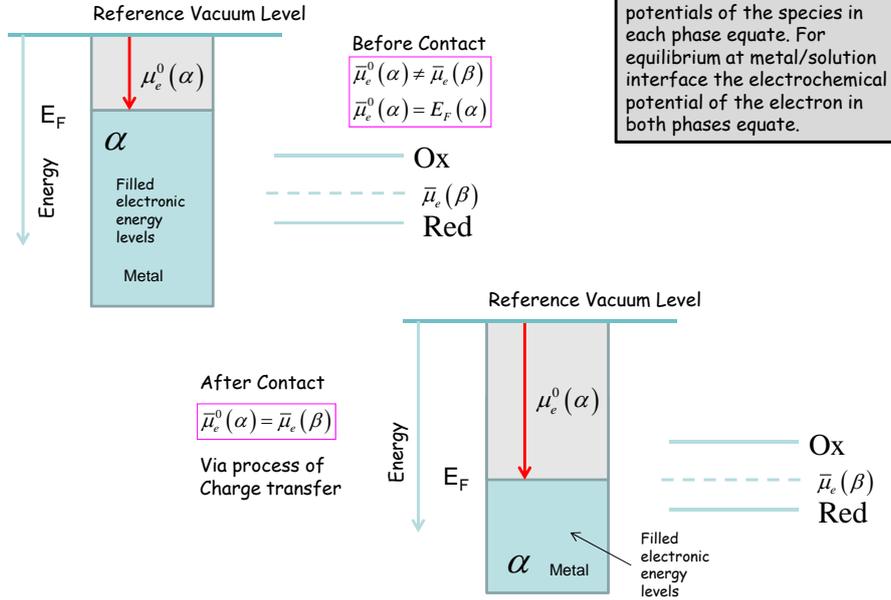
$$= \Delta \mu_i + z_i F \Delta_{\alpha\beta} \phi$$

Hence the difference in electrochemical potential is split up into two distinct components. First, the difference in chemical potential $\Delta \mu_i$; and second the difference in electrical potential $\Delta_{\alpha\beta} \phi$.

Hence we note that the electrochemical potential is defined as the work required to transfer 1 mole of charged species from infinity in vacuum into a material phase. This work consists of three separate terms. The first constitutes a chemical term which includes all short range interactions between species (such as an ion) and its environment (ion/dipole interaction, ion/induced dipole interactions, dispersion forces etc). This constitutes the chemical potential term μ_i . The second constitutes an electrostatic term linked to the crossing of the layer of oriented interfacial dipoles ($z_i F \chi$). The third constitutes an electrostatic term linked to the charge of the phase ($z_i F \psi$). The outer potential ψ is the work done in bringing a test charge from infinity up to a point outside a phase where the influence of short range image forces can be neglected. The surface potential χ defines the work done to bring a test charge across the surface layer of oriented dipoles at the interface. Hence the inner Galvani potential f is then defined as the work done to bring the test charge from infinity to the inside of the phase in question and so we define:

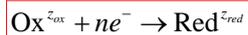
$$\phi = \chi + \psi$$

Rigorous Analysis of Electrochemical Equilibrium



The Nernst Equation

We consider the following ET reaction.



$$n = z_{\text{ox}} - z_{\text{red}} = z_{\text{O}} - z_{\text{R}}$$

At equilibrium

$$\bar{\mu}_{\text{O}}(\beta) + n\bar{\mu}_e(\beta) = \bar{\mu}_{\text{R}}(\beta)$$

We note the following

$$\bar{\mu}_e(\beta) = \mu_e^0 - F\phi_\beta$$

$$\bar{\mu}_{\text{O}}(\beta) = \mu_{\text{O}}(\beta) + z_{\text{O}}F\phi_\beta$$

$$\bar{\mu}_{\text{R}}(\beta) = \mu_{\text{R}}(\beta) + z_{\text{R}}F\phi_\beta$$

Also

$$\mu_{\text{O}}(\beta) = \mu_{\text{O}}^0(\beta) + RT \ln a_{\text{O}}(\beta)$$

$$\mu_{\text{R}}(\beta) = \mu_{\text{R}}^0(\beta) + RT \ln a_{\text{R}}(\beta)$$

Hence

$$\begin{aligned} \mu_{\text{O}}^0(\beta) + RT \ln a_{\text{O}}(\beta) + n\bar{\mu}_e(\beta) + z_{\text{O}}F\phi_\beta \\ = \mu_{\text{R}}^0(\beta) + RT \ln a_{\text{R}}(\beta) + z_{\text{R}}F\phi_\beta \end{aligned}$$

Simplifying we get

$$n\bar{\mu}_e(\beta) = \mu_{\text{R}}^0(\beta) - \mu_{\text{O}}^0(\beta) + RT \ln \left\{ \frac{a_{\text{R}}(\beta)}{a_{\text{O}}(\beta)} \right\} + (z_{\text{R}} - z_{\text{O}})F\phi_\beta$$

$$n\bar{\mu}_e(\beta) = \mu_{\text{R}}^0(\beta) - \mu_{\text{O}}^0(\beta) + RT \ln \left\{ \frac{a_{\text{R}}(\beta)}{a_{\text{O}}(\beta)} \right\} - nF\phi_\beta$$

Hence

$$\bar{\mu}_e(\beta) = \frac{\mu_{\text{R}}^0(\beta) - \mu_{\text{O}}^0(\beta)}{n} + \frac{RT}{n} \ln \left\{ \frac{a_{\text{R}}(\beta)}{a_{\text{O}}(\beta)} \right\} - F\phi_\beta$$

Also

$$\bar{\mu}_e(\alpha) = \mu_e^0(\alpha) - F\phi_\alpha$$

At equilibrium

$$\bar{\mu}_e(\beta) = \bar{\mu}_e(\alpha)$$

Simplifying we get

$$\phi_\alpha - \phi_\beta = \frac{\mu_{\text{O}}^0(\beta) - \mu_{\text{R}}^0(\beta) + n\mu_e^0(\alpha)}{nF} + \frac{RT}{nF} \ln \left\{ \frac{a_{\text{O}}(\beta)}{a_{\text{R}}(\beta)} \right\}$$

$$\Delta_{\alpha\beta}\phi = \Delta_{\alpha\beta}\phi^0 + \frac{RT}{nF} \ln \left\{ \frac{a_{\text{O}}(\beta)}{a_{\text{R}}(\beta)} \right\}$$

$$\Delta_{\alpha\beta}\phi^0 = \frac{\mu_{\text{O}}^0(\beta) - \mu_{\text{R}}^0(\beta) + n\mu_e^0(\alpha)}{nF}$$

This is the Nernst Equation.

Review of Thermodynamics

We recall that the Gibbs energy G is used to determine whether a chemical reaction proceeds spontaneously or not. We consider the gas phase reaction $A(g) \rightarrow B(g)$. We let ξ denote the extent of reaction. Clearly $0 < \xi < 1$. When $\xi = 0$ we have pure A and when $\xi = 1$ we have 1 mol A destroyed and 1 mol B formed.

Also $dn_A = -d\xi$ and $dn_B = +d\xi$ where n denotes the quantity (mol) of material used up or formed. By definition the change in Gibbs energy dG at constant T and P is related to the chemical potential μ as follows:

$$dG = \mu_A dn_A + \mu_B dn_B = -\mu_A d\xi + \mu_B d\xi = (\mu_B - \mu_A) d\xi \quad (1)$$

Furthermore

$$dG = \left(\frac{\partial G}{\partial \xi} \right)_{P,T} d\xi \quad (2)$$

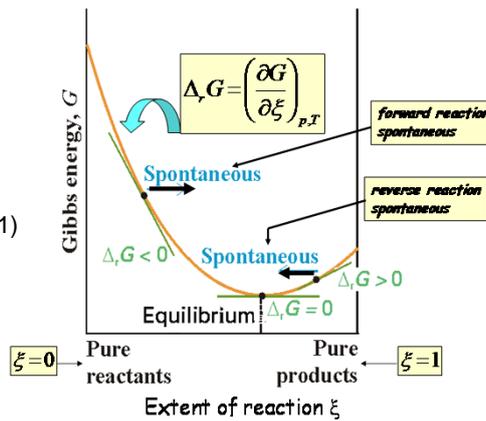
Hence we get from eqn. 1 and 2

$$\left(\frac{\partial G}{\partial \xi} \right)_{P,T} = \Delta_r G = \mu_B - \mu_A \quad (3)$$

In the latter the symbol $\Delta = \frac{\partial}{\partial \xi}$

$\Delta_r G$ = reaction Gibbs free energy

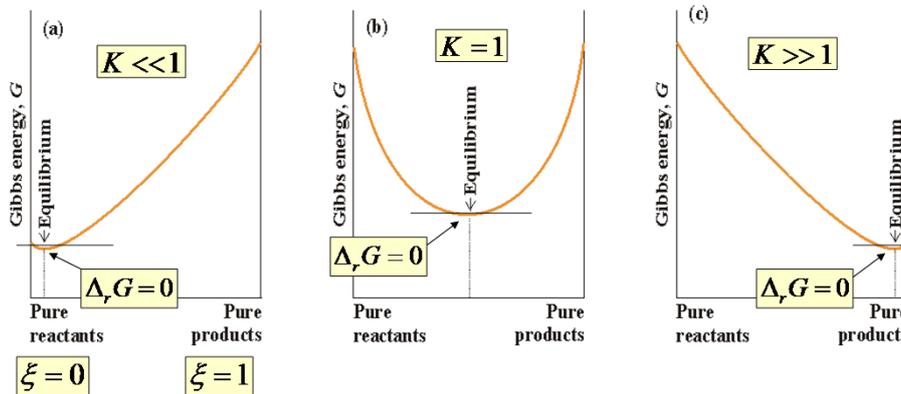
Since μ_j varies with composition Then so also does $\Delta_r G$.



Reaction Gibbs energy

$$\Delta_r G = \left(\frac{\partial G}{\partial \xi} \right)_{P,T}$$

extent of reaction = ξ



$\Delta_r G$ is the slope of the G versus ξ graph at any degree of advancement ξ of the chemical reaction.

If $\mu_A > \mu_B$ then $A \rightarrow B$ is spontaneous and $\Delta_r G$ is negative.
 If $\mu_A < \mu_B$ then $B \rightarrow A$ is spontaneous and $\Delta_r G$ is positive.
 If $\mu_A = \mu_B$ then $\Delta_r G = 0$ and chemical equilibrium has been achieved.

Since A and B are ideal gases then we write

$$\begin{aligned}\mu_A &= \mu_A^0 + RT \ln \frac{p_A}{p^0} \\ \mu_B &= \mu_B^0 + RT \ln \frac{p_B}{p^0} \\ \mu_B - \mu_A &= \mu_B^0 - \mu_A^0 + RT \ln \left(\frac{p_B}{p^0} \right) - RT \ln \left(\frac{p_A}{p^0} \right) \\ &= \mu_B^0 - \mu_A^0 + RT \ln \left(\frac{p_B}{p_A} \right) \\ &= \Delta_r G^0 + RT \ln Q_R\end{aligned}$$

Q_R = reaction quotient
 K = Equilibrium constant

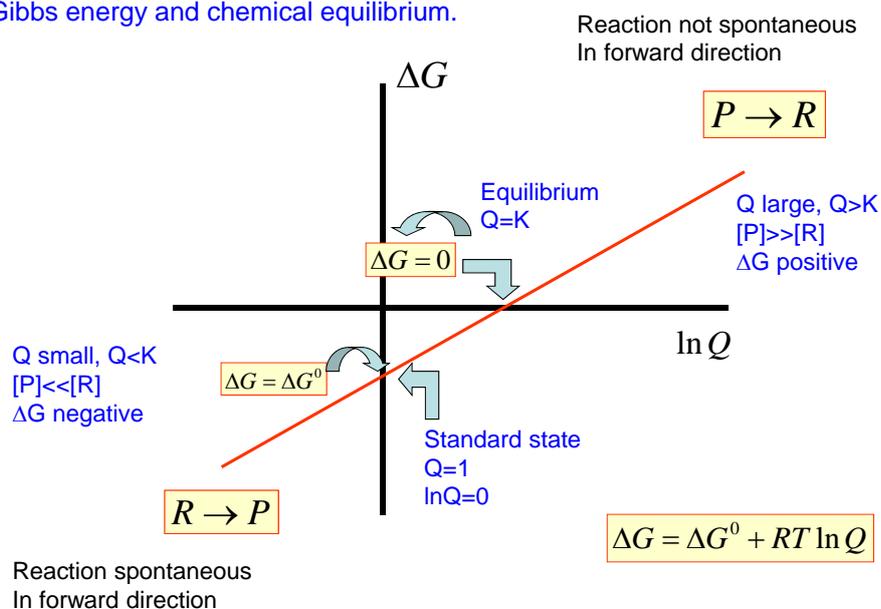
$$\Delta_r G = -RT \ln K + RT \ln Q_R = RT \ln \left(\frac{Q_R}{K} \right)$$

$$\Delta_r G = \Delta_r G^0 + RT \ln Q_R$$

At equilibrium $Q_R = K$ and $\Delta_r G = 0$

$$\Delta_r G = -RT \ln K$$

Gibbs energy and chemical equilibrium.



The expression just derived for the special case $A \rightarrow B$ can also be derived more generally. If we set ν_j as the stoichiometric coefficient of species j (negative for reactants and positive for products, we can derive the following.

$$dG = \sum_j \nu_j \mu_j d\xi = \left(\frac{\partial G}{\partial \xi} \right)_{P,T} d\xi$$

$$\Delta_r G = \left(\frac{\partial G}{\partial \xi} \right)_{P,T} = \sum_j \nu_j \mu_j$$

We can relate chemical potential μ_j to activity a_j as follows.

$$\mu_j = \mu_j^0 + RT \ln a_j$$

In the latter we have introduced the following definitions.

$$Q_R = \prod_j a_j^{\nu_j}$$

$$\sum_j \ln a_j^{\nu_j} = \ln \left\{ \prod_j a_j^{\nu_j} \right\}$$

$$\Delta_r G = \sum_j \nu_j \mu_j^0 + RT \sum_j \nu_j \ln a_j$$

$$= \Delta_r G^0 + RT \sum_j \ln a_j^{\nu_j}$$

$$= \Delta_r G^0 + RT \ln \left\{ \prod_j a_j^{\nu_j} \right\}$$

$$\Delta_r G = \Delta_r G^0 + RT \ln Q_R$$

Again at equilibrium

$$\Delta_r G = 0 \quad Q_R = K$$

$$\Delta_r G^0 = -RT \ln K$$

$$K = \prod_j a_j^{\nu_j}$$

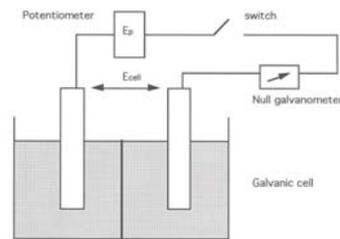
$$\Delta_r G^0 = \sum_j \nu_j \Delta_f G^0$$

$$\Delta_f G^0 =$$

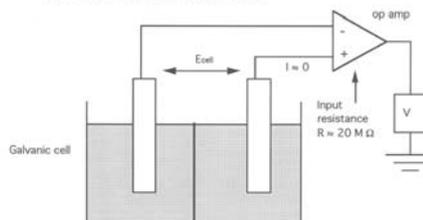
Standard free energy of formation of species j .

Potentiometric Measurements

We now mention the practicalities of conducting a potentiometric measurement. A two electrode electrochemical cell is used. This consists of a reference electrode and an indicator electrode. The object of the exercise is to make a measurement of the equilibrium cell potential without drawing any significant current since we note that the equilibrium cell potential is defined as $E = \Delta\phi_{(i \rightarrow 0)}$ where $\Delta\phi$ denotes the Galvani potential difference measured between the cell terminals. This objective is achieved either using a null detecting potentiometer or a high impedance voltmeter.



Classical method: The voltage E_p is manually adjusted until it equals E_{cell} and the galvanometer reads zero deflection. This method is based on the principle of voltage compensation and is still used for high precision measurements.



Modern method uses an electronic voltage follower based on operational amplifier circuits (digital voltmeter DVM). The voltage follower reproduces the cell voltage E_{cell} and does not draw any significant current from the cell since its input impedance is very large.

The second measurement protocol involves use of an electrometer. The latter is based on a voltage follower circuit. A voltage follower employs an operational amplifier. The amplifier has two input terminals called the summing point S (or inverting input) and the follower input F (or non-inverting input). Note that the positive or negative signs at the input terminals do not reflect the input voltage polarity but rather the non-inverting and inverting nature respectively of the inputs. Now the fundamental property of the operational amplifier is that the output voltage V_o is the inverted, amplified voltage difference V_Δ where $V_\Delta = V_- - V_+$ denotes the voltage of the inverting input with respect to the non-inverting input. Hence we can write that

$$V_o = -AV_- + AV_+ = -AV_\Delta$$

In the latter A denotes the open loop gain of the amplifier. Although ideally A should be infinite it will typically be 10^5 .

$$V_o = -AV_\Delta = -A(V_o - V_i)$$

$$V_o = \frac{V_i}{1 + \frac{1}{A}} \approx V_i$$

Also ideally the amplifier should exhibit an infinite input impedance so that they can accept input voltages without drawing any current from the voltage source. This is why we can measure a voltage without any perturbation. In practice the input impedance will be large but finite (typically $10^6 \Omega$). An ideal amplifier should also be able to supply any desired current to a load. The output impedance should be zero. In practice amplifiers can supply currents in the mA range although higher current output can also be achieved.

Keeping these comments in mind we can now discuss the operation of the voltage follower circuit presented. In this configuration the entire output voltage is returned to the inverting input. If V_i represents the input voltage then we see from the analysis outlined across that the circuit is called a voltage follower because the output voltage is the same as the input voltage. The circuit offers a very high input impedance and a very low output impedance and can therefore be used to measure a voltage without perturbing the voltage significantly.

The Nernst equation.

The potential developed by a Galvanic cell depends on the composition of the cell.

From thermodynamics the Gibbs energy change for a chemical reaction ΔG varies with composition of the reaction mixture in a well defined manner. We use the relationship between ΔG and E to obtain the Nernst equation.

$$\Delta_r G = -nFE \quad \Delta_r G^0 = -nFE^0$$

$$-nFE = -nFE^0 + RT \ln Q_R$$

$$\Delta_r G = \Delta_r G^0 + RT \ln Q_R$$

$$RT/F = 25.7 \text{ mV}$$

$$\text{At } T = 298 \text{ K}$$

Reaction quotient

$$Q_R \cong \frac{[\text{products}]}{[\text{reactants}]}$$

$$E = E^0 - \frac{RT}{nF} \ln Q_R$$

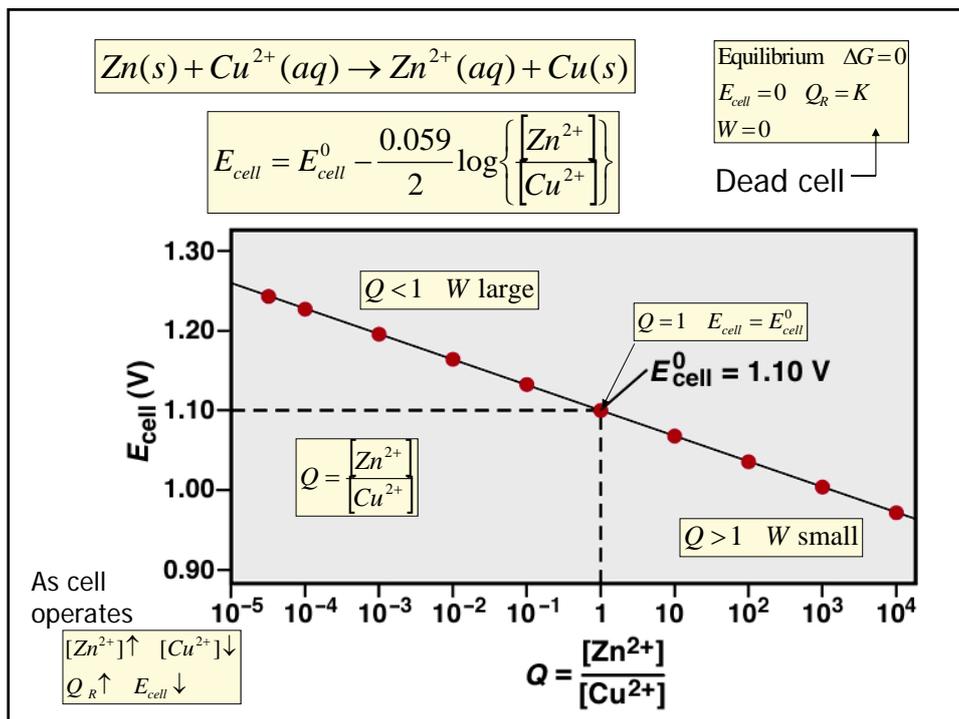
$T = 298 \text{ K}$

$$E = E^0 - \frac{0.0592}{n} \log Q_R$$

Walther Hermann Nernst



Nernst eqn. holds for single redox couples and net cell reactions.



Determination of thermodynamic parameters from E_{cell} vs temperature data.

Measurement of the zero current cell potential E as a function of temperature T enables thermodynamic quantities such as the reaction enthalpy ΔH and reaction entropy ΔS to be evaluated for a cell reaction.

$$E = a + b(T - T_0) + c(T - T_0)^2 + \dots$$

a , b and c etc are constants, which can be positive or negative.

T_0 is a reference temperature (298K)

$$\left(\frac{\partial E}{\partial T} \right)_P$$

← Temperature coefficient of zero current cell potential obtained from experimental $E = E(T)$ data. Typical values lie in range $10^{-4} - 10^{-5} \text{ VK}^{-1}$

Gibbs-Helmholtz eqn.

$$\Delta_r H = \Delta_r G - T \left(\frac{\partial \Delta_r G}{\partial T} \right)_P$$

$$\begin{aligned} \Delta_r H &= -nFE - T \left\{ \frac{\partial (-nFE)}{\partial T} \right\} \\ &= -nFE + nFT \left(\frac{\partial E}{\partial T} \right)_P \end{aligned}$$

$$\Delta_r G = -nFE$$

$$\Delta_r H = -nF \left\{ E - T \left(\frac{\partial E}{\partial T} \right)_P \right\}$$

- Once ΔH and ΔG are known then ΔS may be evaluated.

$$\Delta_r G = \Delta_r H - T \Delta_r S$$

$$\Delta_r S = \frac{\Delta_r H - \Delta_r G}{T}$$

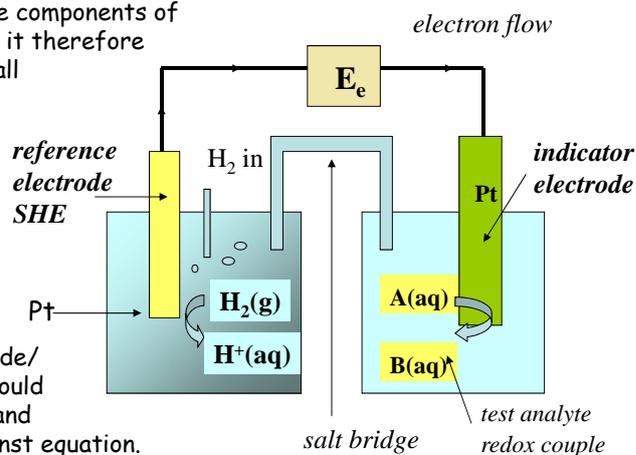
$$\Delta_r S = \frac{1}{T} \left\{ -nFE + nFT \left(\frac{\partial E}{\partial T} \right)_p + nFE \right\}$$

$$\Delta_r S = nF \left(\frac{\partial E}{\partial T} \right)_p$$

- Electrochemical measurements of cell potential conducted under conditions of zero current flow as a function of temperature provide a sophisticated method of determining useful thermodynamic quantities.

Fundamentals of potentiometric measurement : the Nernst Equation.

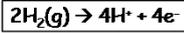
The potential of the indicator electrode is related to the activities of one or more of the components of the test solution and it therefore determines the overall equilibrium cell potential E_e . Under ideal circumstances, the response of the indicator electrode to changes in analyte species activity at the indicator electrode/solution interface should be rapid, reversible and governed by the Nernst equation.



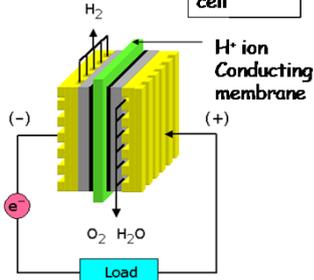
The ET reaction involving the analyte species should be kinetically facile and the ratio of the analyte/product concentration should depend on the interfacial potential difference via the Nernst equation.

Hydrogen/oxygen fuel cell

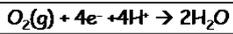
Anode reaction



H_2/O_2 fuel cell



Cathode reaction



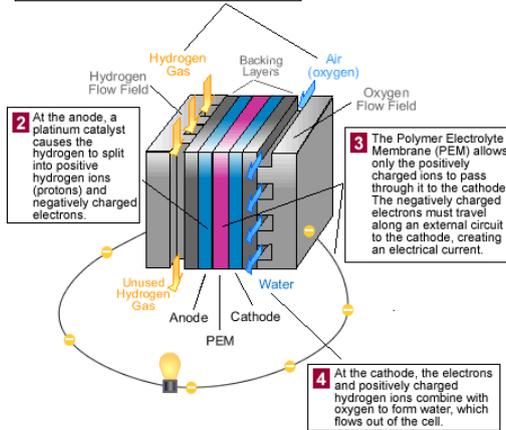
Remember CH1101
Electrochemistry:

1 Hydrogen fuel is channeled through field flow plates to the anode on one side of the fuel cell, while oxygen from the air is channeled to the cathode on the other side of the cell.

2 At the anode, a platinum catalyst causes the hydrogen to split into positive hydrogen ions (protons) and negatively charged electrons.

3 The Polymer Electrolyte Membrane (PEM) allows only the positively charged ions to pass through it to the cathode. The negatively charged electrons must travel along an external circuit to the cathode, creating an electrical current.

4 At the cathode, the electrons and positively charged hydrogen ions combine with oxygen to form water, which flows out of the cell.

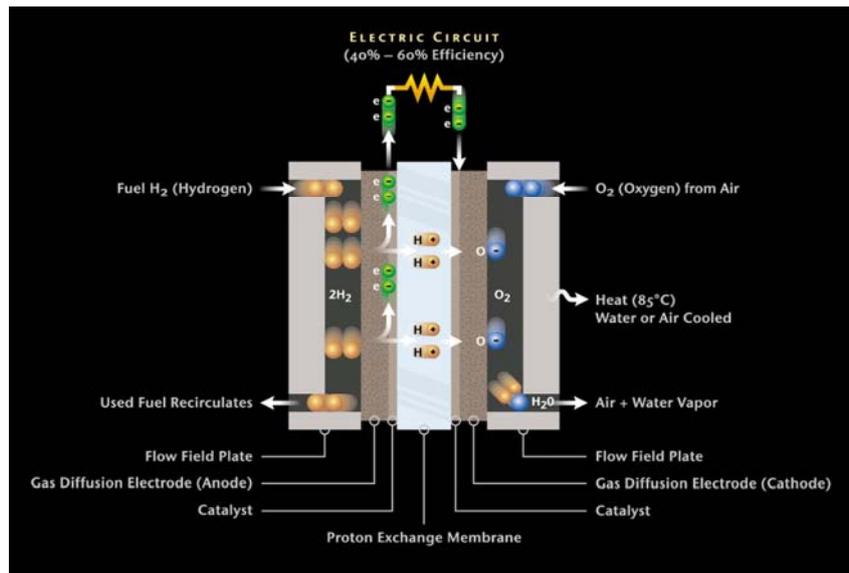


A fuel cell consists of two electrodes sandwiched around an electrolyte

$$\Delta G = -nFE_{eq,cell}$$

$$E_{eq,cell} = E_{eq,C} - E_{eq,A}$$

Ballard PEM Fuel Cell.



Efficiency of fuel cell(I) .

Efficiency ε = work output/heat input

$$\Delta G = -nFE_{eq,cell}$$

$$E_{eq,cell} = E_{eq,C} - E_{eq,A}$$

For electrochemical or 'cold' combustion:

Heat input \rightarrow enthalpy change ΔH for cell reaction

Work output \rightarrow Gibbs energy change ΔG for cell reaction

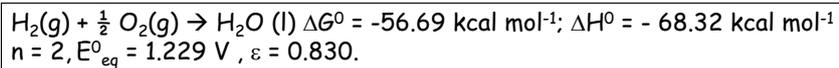
$$\varepsilon_{max} = \frac{\Delta_r G}{\Delta_r H} = \frac{\Delta_r H - T\Delta_r S}{\Delta_r H} = 1 - \frac{T\Delta_r S}{\Delta_r H}$$

$$\varepsilon_{max} = -\frac{nFE_{eq,cell}}{\Delta_r H}$$

Usually

$$\Delta_r G \cong \Delta_r H$$

$$\varepsilon \cong 1$$



Efficiency of fuel cell (II).

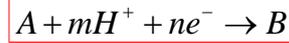
- For all real fuel cell systems terminal cell potential E does not equal the equilibrium value E_{eq} , but will be less than it.
- Furthermore E will decrease in value with increasing current drawn from the fuel cell.
- This occurs because of:
 - Slowness of one or more intermediate steps of reactions occurring at one or both electrodes.
 - Slowness of mass transport processes either reactants to, or products from, the electrodes.
 - Ohmic losses through the electrolyte.

$$\varepsilon_{real} = -\frac{nFE_{cell}}{\Delta H} = -\frac{nF(E_{eq} - \sum |\eta|)}{\Delta H}$$

Sum of all overpotential Losses.

Nernst Equation involving both an electron and proton transfer.

We consider the following reaction which involves both the transfer of m protons and n electrons. This is a situation often found in biochemical and organic reactions.

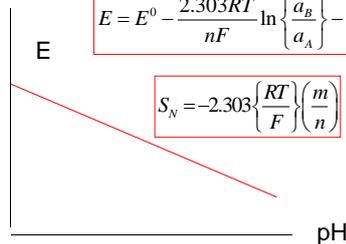


The Nernst equation for this type of proton/electron transfer equilibrium is given by the following expression.

$$E = E^0 - \frac{RT}{nF} \ln \left\{ \frac{a_B}{a_A a_{H^+}^m} \right\}$$

This expression can be readily simplified to the following form

$$E = E^0 - \frac{2.303RT}{nF} \ln \left\{ \frac{a_B}{a_A} \right\} - 2.303 \left(\frac{m}{n} \right) \frac{RT}{F} pH$$



$$S_N = -2.303 \left(\frac{RT}{F} \right) \left(\frac{m}{n} \right)$$

Hence we predict that a Nernst plot of open circuit or equilibrium Potential versus solution pH should be linear With a Nernst slope S_N whose value is directly related to the redox stoichiometry of the redox reaction through the m/n ratio. When m = n then we predict that $S_N = -2/303RT/F$ Which is close to 60 mV per unit change in pH at 298 K.

Idea: Potentiometric measurements can give rise to accurate pH measurements (especially metal oxide electrodes Lyons TEECE Group Research 2012/2013).

Membrane Potential

Since we are considering charged species we define equilibrium in terms of equality of electrochemical potentials.

$$\bar{\mu}_j(\alpha) = \bar{\mu}_j(\beta)$$

$$\mu_j(\alpha) + z_j F \phi_\alpha = \mu_j(\beta) + z_j F \phi_\beta$$

$$\Delta_{\beta\alpha} \phi = \phi_\beta - \phi_\alpha > 0 \quad \begin{matrix} a_j(\alpha) > a_j(\beta) \\ \phi_\alpha < \phi_\beta \end{matrix}$$

$$z_j F \phi_\beta - z_j F \phi_\alpha = z_j F (\phi_\beta - \phi_\alpha) = \mu_j(\alpha) - \mu_j(\beta)$$

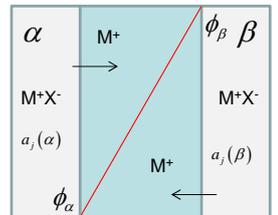
Now
$$\begin{aligned} \mu_j(\alpha) &= \mu_j^0(\alpha) + RT \ln a_j(\alpha) \\ \mu_j(\beta) &= \mu_j^0(\beta) + RT \ln a_j(\beta) \end{aligned}$$

Hence

$$\begin{aligned} z_j F (\phi_\beta - \phi_\alpha) &= (\mu_j^0(\alpha) - \mu_j^0(\beta)) + RT \ln a_j(\alpha) - RT \ln a_j(\beta) \\ &= (\mu_j^0(\alpha) - \mu_j^0(\beta)) + RT \ln \left\{ \frac{a_j(\alpha)}{a_j(\beta)} \right\} \\ \Delta_{\beta\alpha} \phi &= \frac{(\mu_j^0(\alpha) - \mu_j^0(\beta))}{z_j F} + \frac{RT}{z_j F} \ln \left\{ \frac{a_j(\alpha)}{a_j(\beta)} \right\} \end{aligned}$$

$\Delta\phi$ is the electric potential necessary To prevent equalization of ionic activities by Diffusion across the membrane.

Of course a similar result for the membrane potential can be obtained by equalizing the ratio of electrochemical activities and noting that the following pertains.



Net - ve ← → Net + ve

δ

Membrane permeable only to M^+ ion.

Now if we assume that $\mu_j^0(\alpha) = \mu_j^0(\beta)$

We get the final expression for the membrane potential

$$\Delta\phi_M = \frac{RT}{z_j F} \ln \left\{ \frac{a_j(\alpha)}{a_j(\beta)} \right\}$$

$$\begin{aligned} \bar{a}_j(\beta)/a_j(\alpha) &= \frac{a_j(\beta)}{a_j(\alpha)} \exp \left[\frac{z_j F}{RT} (\phi_\beta - \phi_\alpha) \right] = 1 \\ \Delta\phi_M &= \frac{RT}{z_j F} \ln \left\{ \frac{a_j(\alpha)}{a_j(\beta)} \right\} \end{aligned}$$